

The Story of (S)-Metolachlor

*An Industrial Odyssey*

*in*

*Asymmetric Catalysis*

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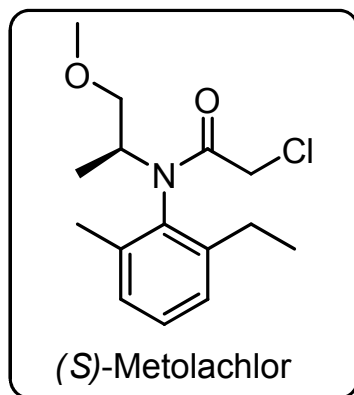
A Literature Presentation

Aman Desai

04.10.09

# The Glory of the Odyssey – Reasons Behind the Talk

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- (S)-metolachlor is the active ingredient in Dual Magnum<sup>®</sup>, one of the most important grass herbicides for use in maize.
- >20,000 ton/year market of the herbicide.
- Key step in synthesis – an Ir-catalyzed asymmetric hydrogenation.
- A 14 year odyssey of development.
- Operated on a >10,000 ton/year scale since 1996.
- This is to date the largest application of asymmetric catalysis.
- The Ir-Xyliphos is the most active and productive catalyst till date (>7,000,000 TON and >2,000,000 TOF).
- Developed during the incipient years of asymmetric hydrogenation – a historical case study.

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Blaser, H-U. *Adv. Synth. Catal.* **2002**, 334, 17-31.

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# Milestones in the History of Metolachlor

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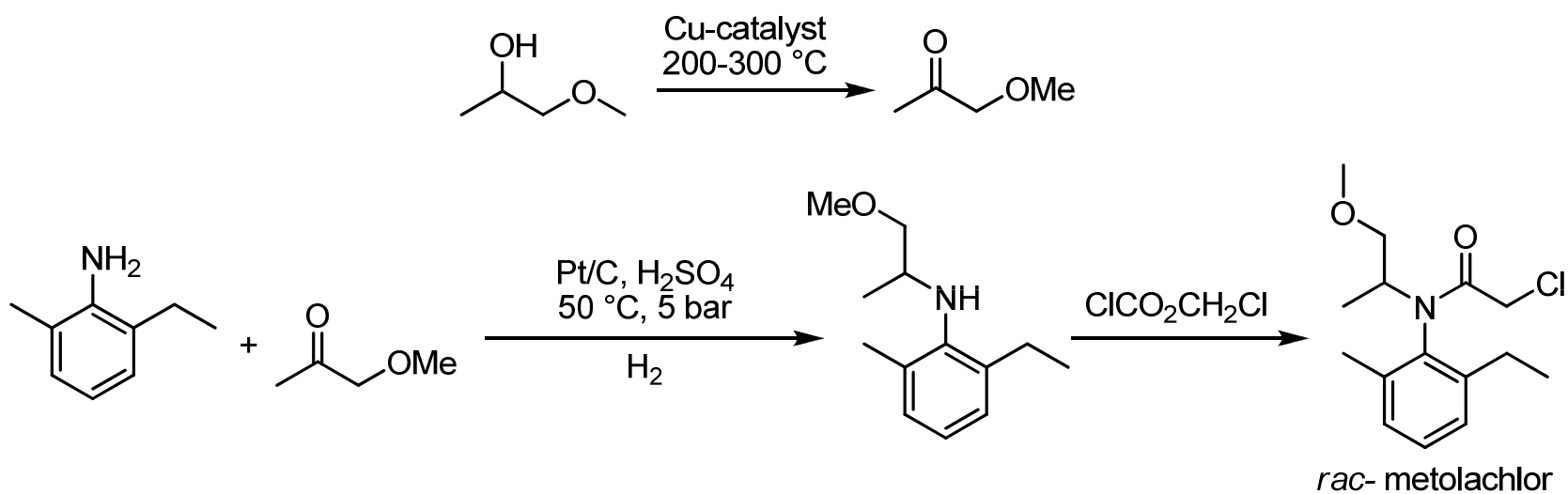
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# The Initial Process for *rac*- Metolachlor

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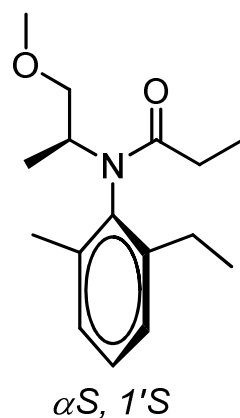
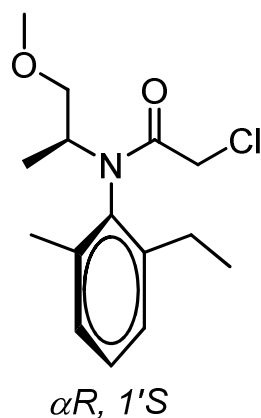
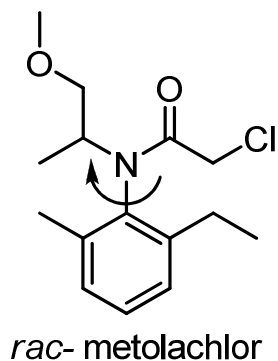
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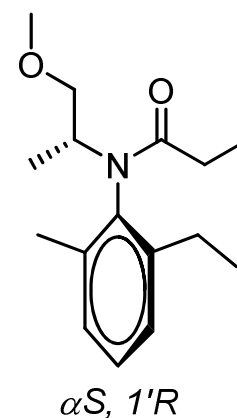
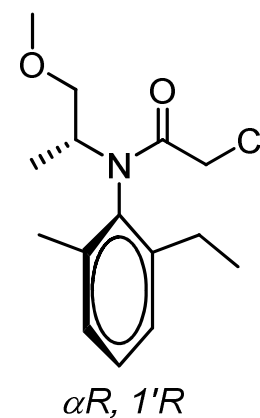
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# Discovery of the Active and Inactive Stereoisomers

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the active stereoisomers



the inactive stereoisomers

95% of herbicidal activity resides in the two ( $1'S$ )-diastereomers.

Thus, same biological effect could be produced at ~60% of the use rate of the racemic product.

*Not a small matter considering the >20,000 t/y market!*

**The quest for a viable commercial catalyst for the asymmetric manufacture had started!**

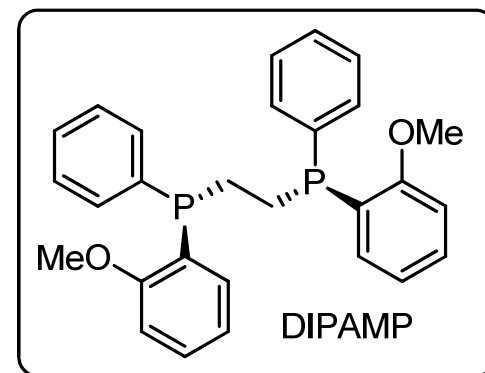
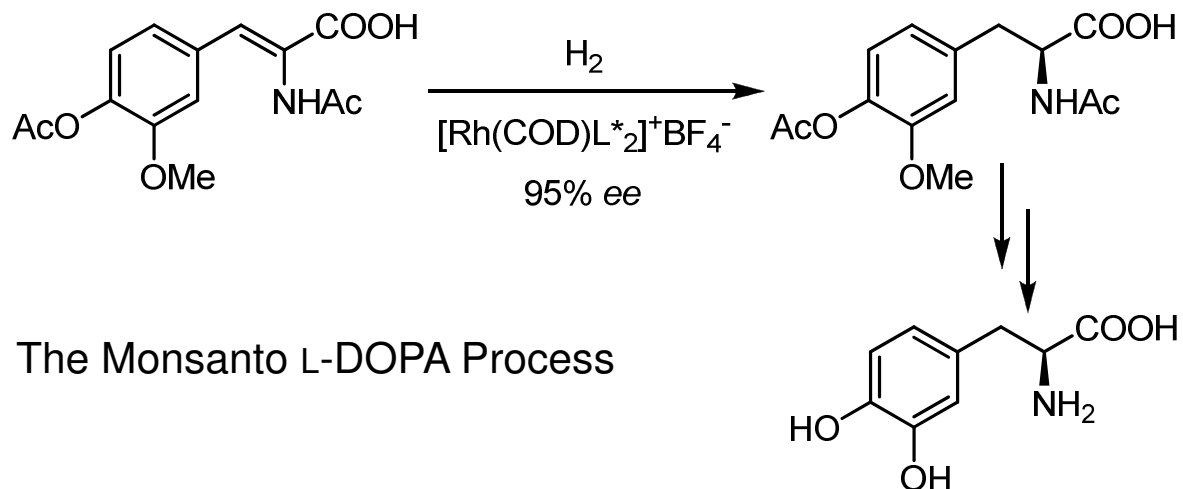
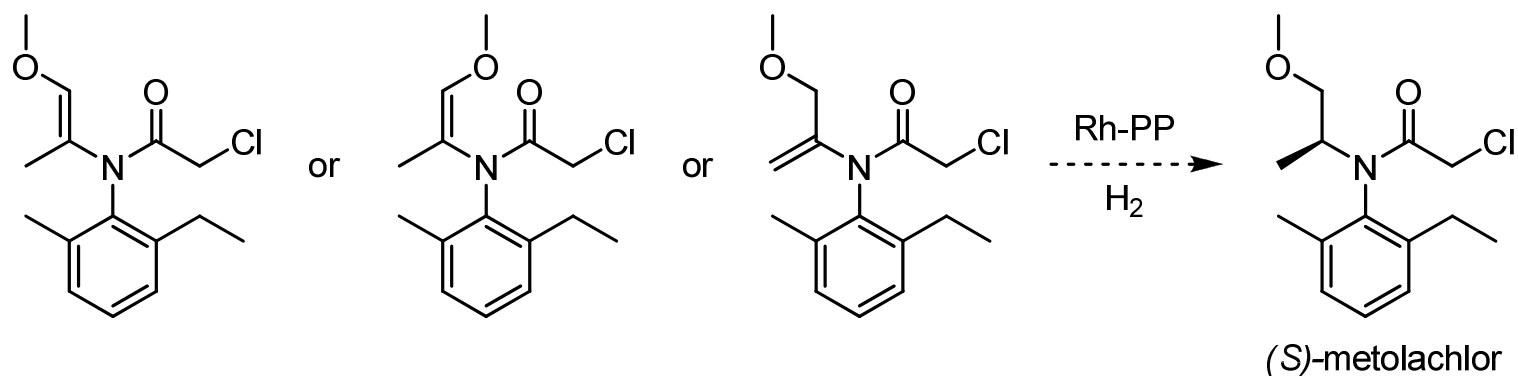
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# The First Assessment and The Four Routes Considered

route	catalytic step	other steps	cost	ecology
enamide	close analogy, <i>ee</i> > 90%	enamide synthesis difficult	high	medium



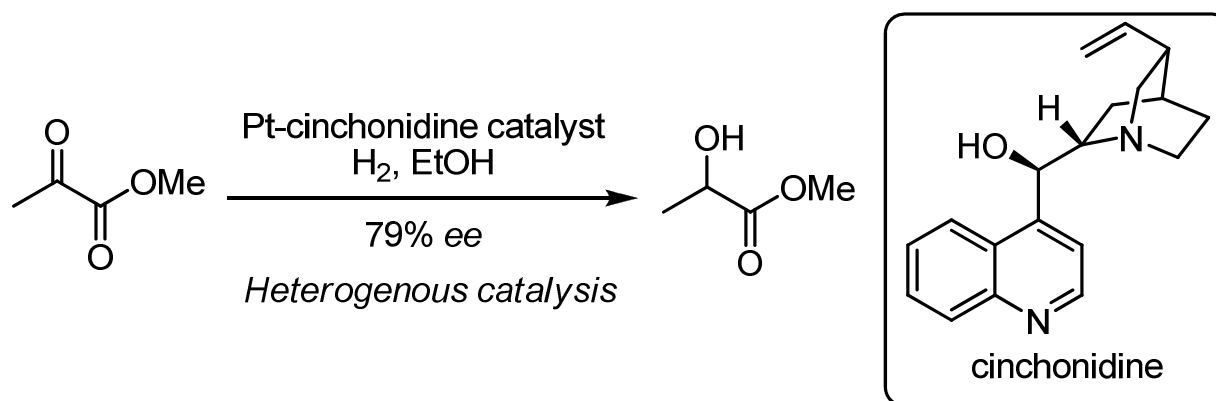
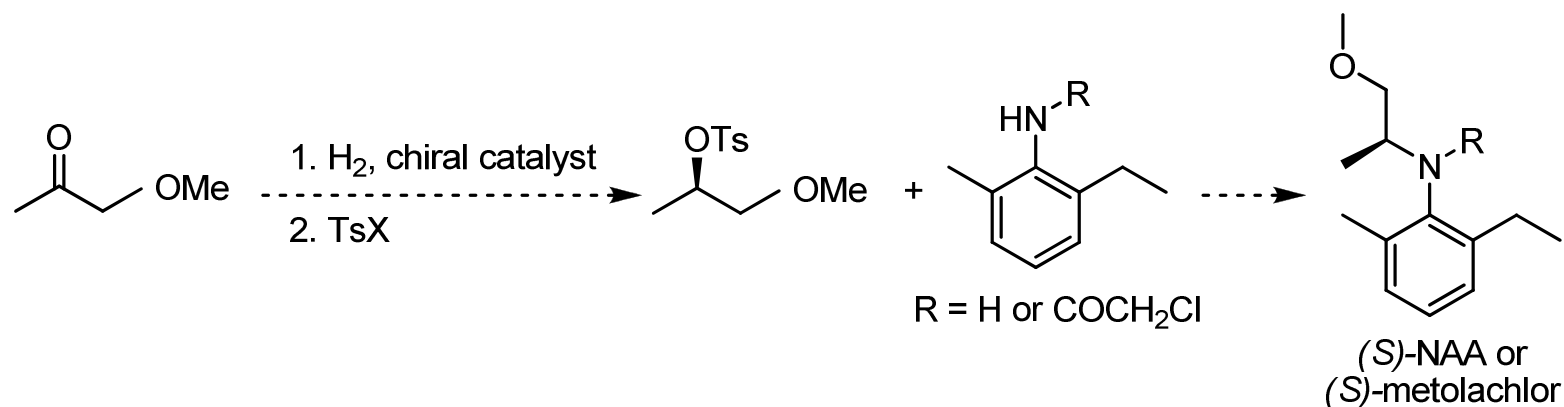
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substitution	weak analogy, <i>ee</i> ~ 80%	substitution very difficult	high	bad

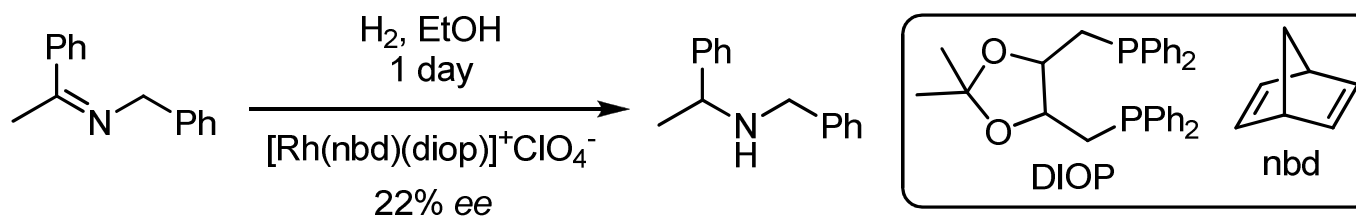
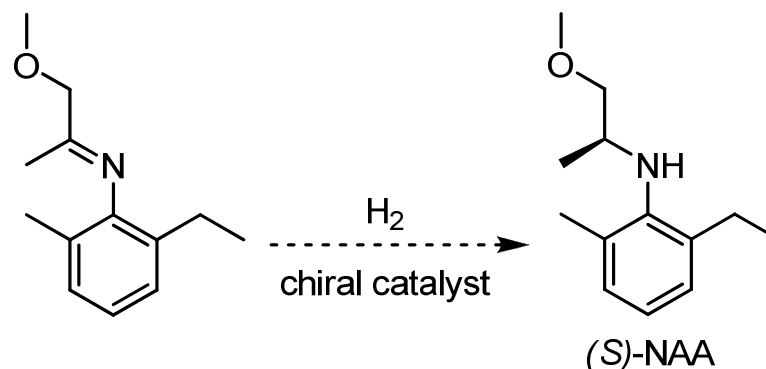


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Orito, Y.; Imai, S.; Niwa, J. *J. Chem. Soc. Jpn.* **1979**, 8, 1118-1120.

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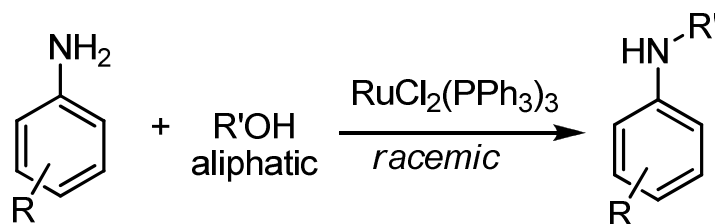
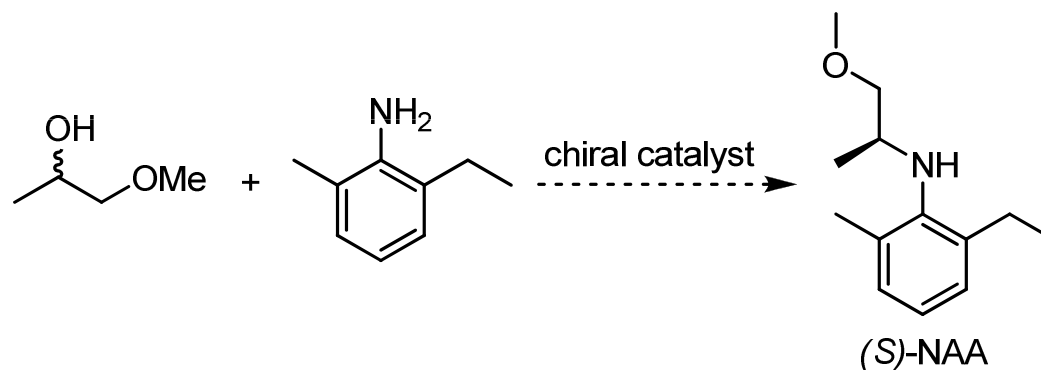


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Levi, A.; Modena, G.; Scorrano, G. *Chem. Commun.* **1975**, 6.

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imine	weak analogy, <i>ee</i> < 30%	as in racemic process	medium	good
direct alkylation	no precedent	as in racemic process	low	very good



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## Priorities Assigned to the Routes

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route	catalytic step	other steps	cost	ecology	priority
enamide	close analogy, <i>ee</i> > 90%	enamide synthesis difficult	high	medium	1
substitution	weak analogy, <i>ee</i> ~ 80%	substitution very difficult	high	bad	2
imine	weak analogy, <i>ee</i> < 30%	as in racemic process	medium	good	3
direct alkylation	no precedent	as in racemic process	low	very good	4

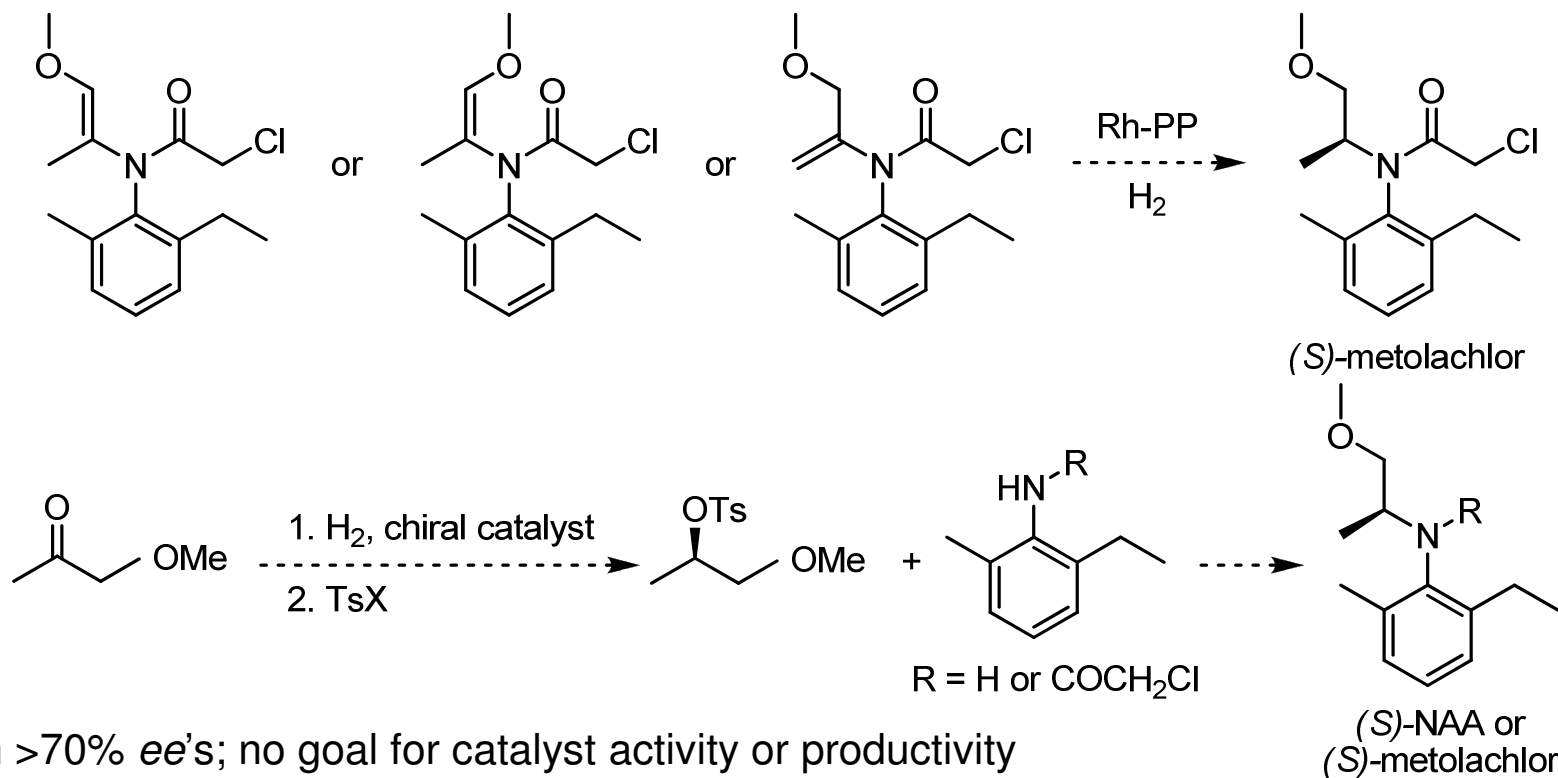
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# Proposed Project and Goals

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enamide	close analogy, $ee > 90\%$	enamide synthesis difficult	high	medium	1
substitution	weak analogy, $ee \sim 80\%$	substitution very difficult	high	bad	2
imine	weak analogy, $ee < 30\%$	as in racemic process	medium	good	3
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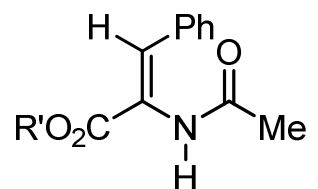


Attain  $>70\%$   $ee$ 's; no goal for catalyst activity or productivity

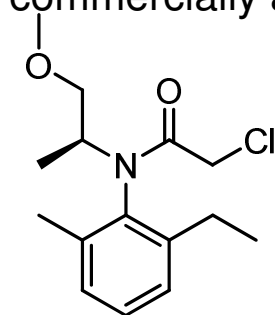
# State of Asymmetric Catalysis in 1981 and at Ciba-Geigy

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- Only one industrial process existed – Monsanto's L-DOPA process.
- Asymmetric enamide hydrogenation: High *ee*'s (>95%), low TON's (<2300), <10 chiral phosphines commercially available (small quantities).



most investigated model



(S)-metolachlor

- Modified heterogeneous catalysts were the most active catalysts for C=O groups. *ee*'s upto 85%.
- No history of asymmetric catalysis at Ciba-Geigy.
- No hydrogenation equipment for homogenous catalysis.

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# The “Theseus-Minotaur” Greek Legend

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*Theseus fighting the Minotaur*  
by Jean-Etienne Ramey, marble, 1826  
Tuileries Gardens, Paris

The ee-TON Labyrinth is the same as the Theseus-Minotaur one

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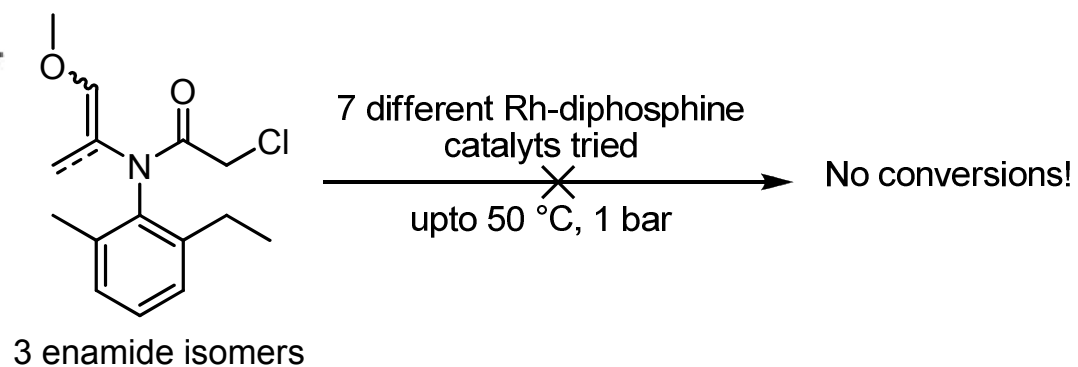


The successful route shown

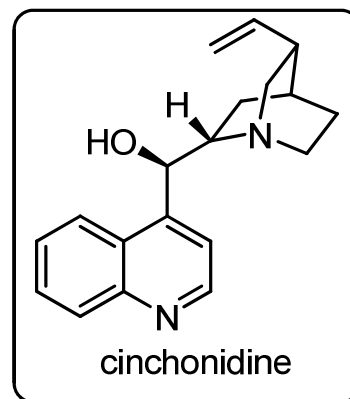
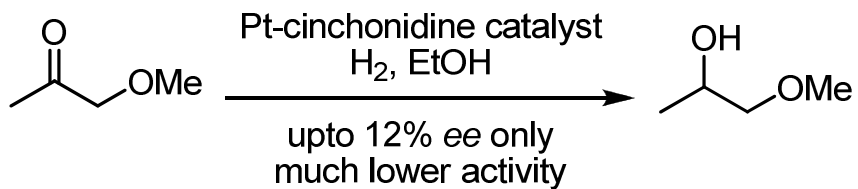
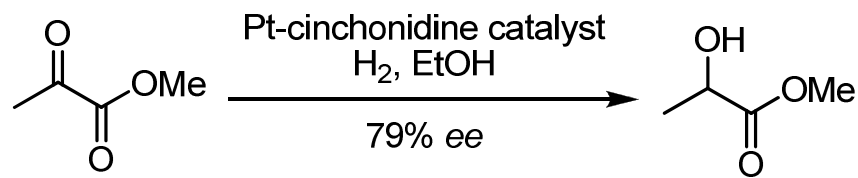
# The First Steps in the Labryinth – the First Disappointments



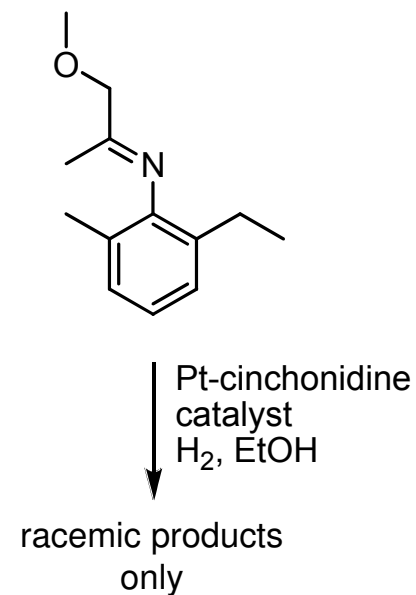
## Enamide hydrogenation route:



## Methoxyacetone reduction route:



## Imine reduction route:



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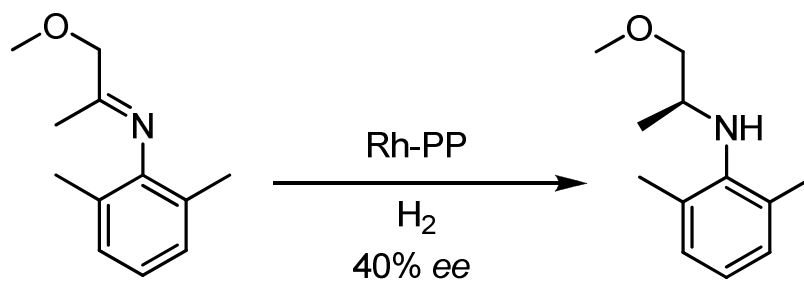
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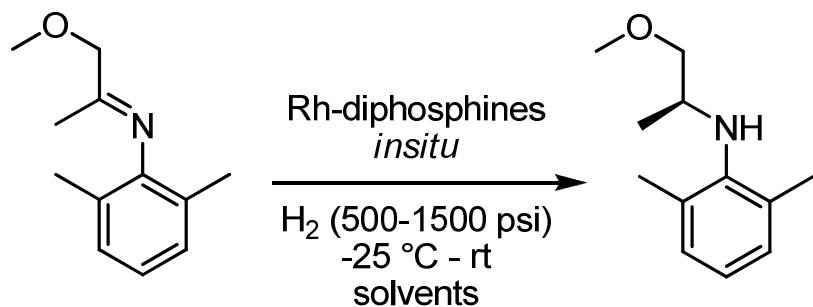
# A Second Chance and the First Breakthrough

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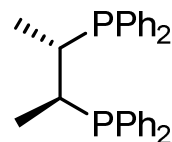
# The U. British-Columbia – Ciba-Geigy Study



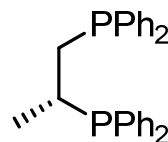
a thorough  
study

0.1 mol% Rh, 0.2 mol% cycphos  
catalyst *insitu*  
-25 °C, 1500 psi H<sub>2</sub>, 70 h, 2:1 MeOH:toluene

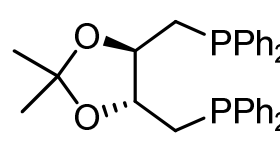
69% ee, 100% conversion  
TOF = 15 h<sup>-1</sup>, TON = 1000



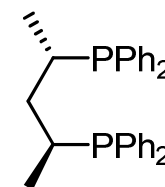
chiraphos  
36% ee



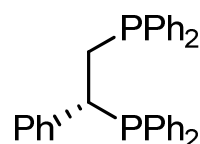
prophos  
38% ee



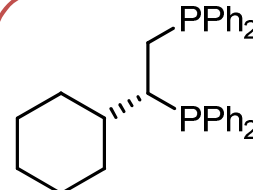
diop  
8% ee



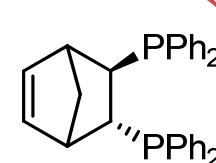
skewphos  
N.R.



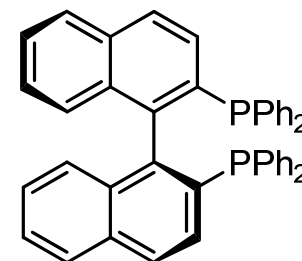
phenphos  
20% ee



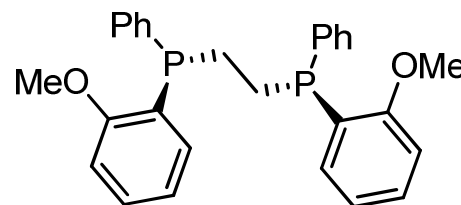
cycphos  
50% ee



norphos  
50% ee



binap  
N.R.



DIPAMP  
24% ee

**ligand screen**  
1 mol% Rh  
rt, 1000 psi H<sub>2</sub>  
Rh-PP *insitu*  
MeOH:C<sub>6</sub>H<sub>6</sub> 1:1

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# The Switch to Iridium Complexes

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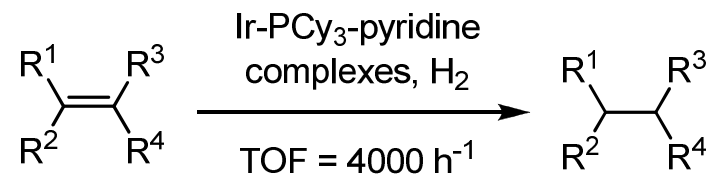
It was thought that Rh-diphosphine complexes would never be active enough.

Best results with Rh – 69% ee, 1000 TON, 70 h

Requirements for a technical process:  $\geq 80\%$  ee,  $> 50,000$  TON,  $< 8$  h

Risks with iridium – very little known, Ir-catalyzed reactions were very rare and none was asymmetric.

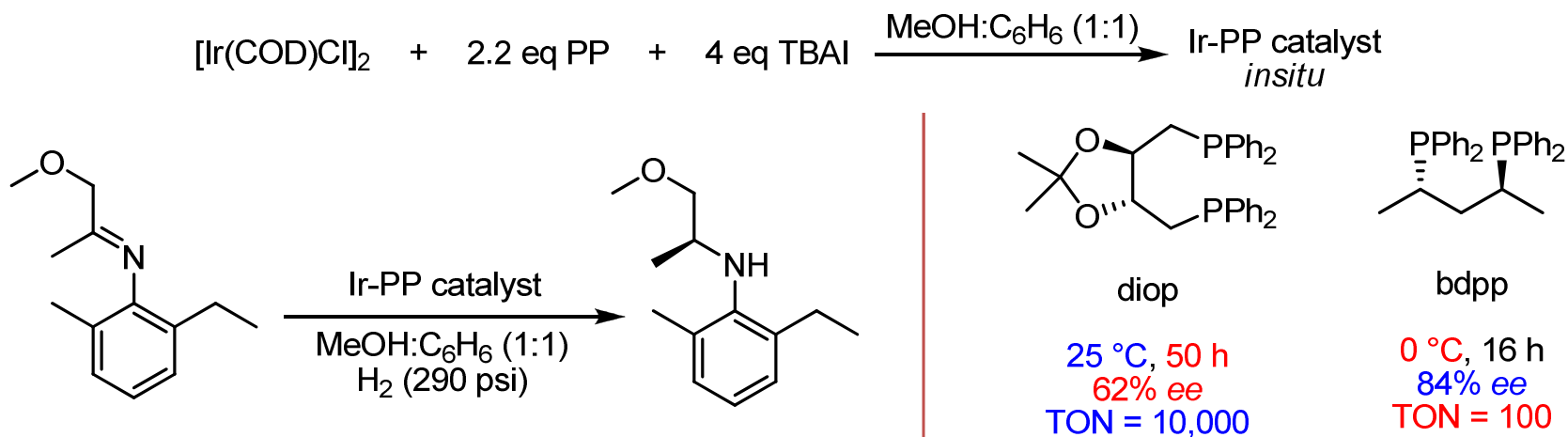
The Crabtree inspiration:



A full study undertaken like the UBC rhodium study.

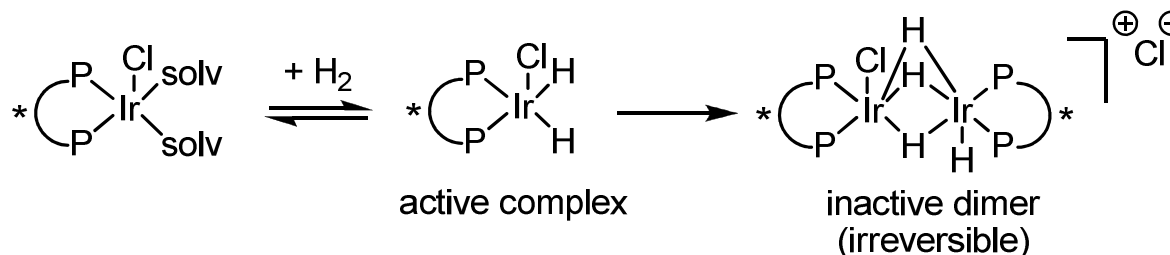


# Good results with Ir – but are they good enough?



Requirements for a technical process:  $\geq 80\%$  ee, TON = 40,000, <8 h

Irreversible catalyst deactivation – a major problem.



This was the best enantioselective imine hydrogenation at that time...

....yet, a new approach was needed.

Splinder, F.; Pugin, B.; Blaser, H-U. *Angew. Chem. Int. Ed. Eng.* **1990**, 29, 588-589.

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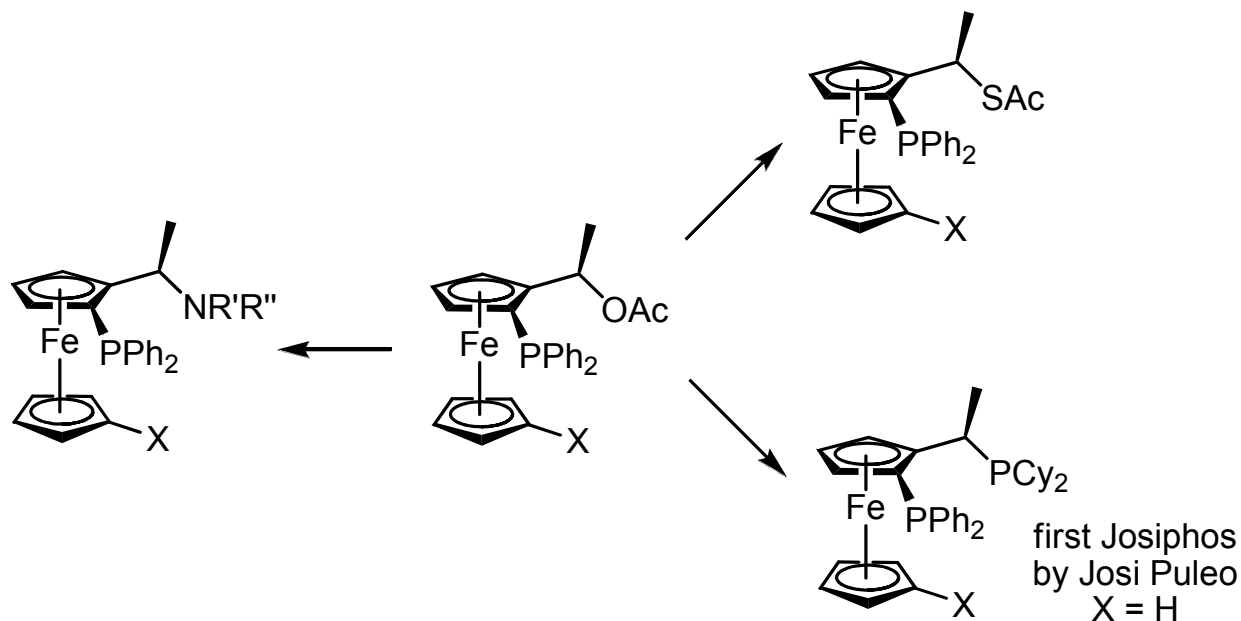
Blaser, H-U. *Adv. Synth. Catal.* **2002**, *334*, 17-31.

Blaser, H-U.; Pugin, B.; Splinder, F.; Thommen, M.; *Acc. Chem. Res.* **2007**, *40*, 1240-1250.

# Josiphos Ligands – A New Family at Ciba-Geigy

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Extremely modular and tunable diphosphine ligands.



From the first try, these ligands were very efficient and were used for several commercial applications.

Numerous new ligands made and screened for (*S*)-metolachlor.

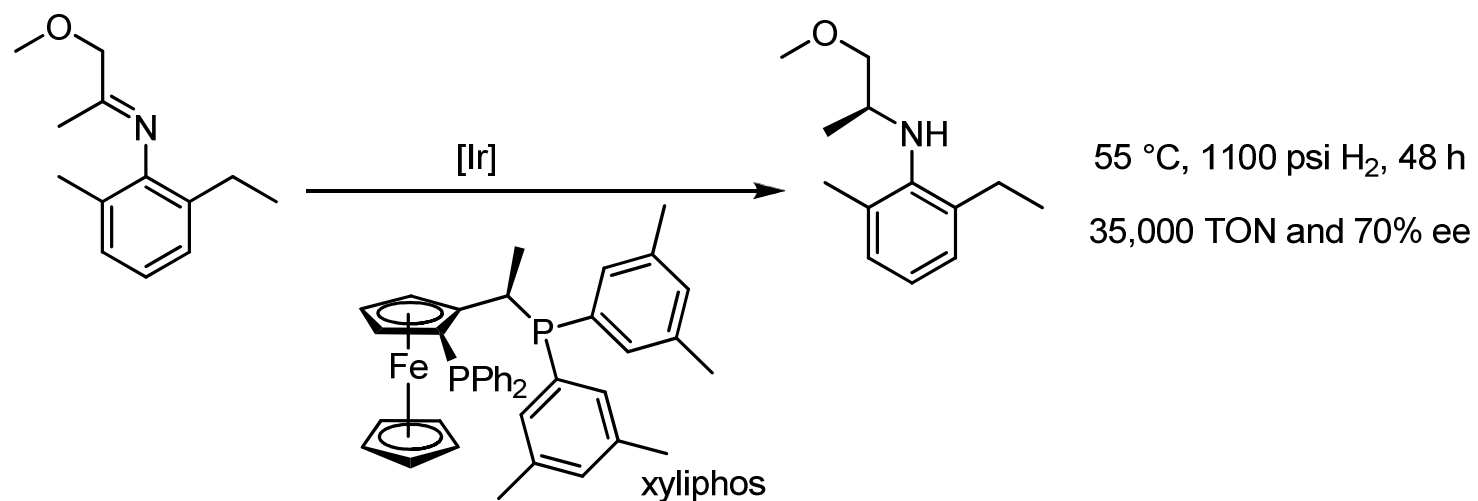
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Blaser, H-U.; Brieden, W.; Pugin, B.; Splinder, F.; Studer, M.; Togni, A. *Top. Cat.* **2002**, *19*, 3-16.

Blaser, H-U. *Adv. Synth. Catal.* **2002**, *334*, 17-31.

# A Third Chance and a Second Breakthrough – Almost There!

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Blaser, H-U. *Adv. Synth. Catal.* **2002**, 334, 17-31.

Blaser, H-U.; Pugin, B.; Splinder, F.; Thommen, M.; *Acc. Chem. Res.* **2007**, 40, 1240-1250.

# Milestones in the History of Metolachlor

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1970	Discovery of the biological activity of metolachlor
1973	Decision to develop a production process
1974	First 100 kg of racemic metolachlor produced
1975/6	Pilot plant in operation (4000 L reactor) and market launch
1978	Full-scale plant with product capacity of >10,000 ton/year in operation
1981	Synthesis & biological tests of the stereoisomers / assessment of routes for chiral synthesis
1983	First unsuccessful attempts to synthesize ( <i>S</i> )-metolachlor via enantioselective catalysis
1985	Rhodium/cycphos catalyst gives 69% <i>ee</i> for the imine hydrogenation (UBC Vancouver)
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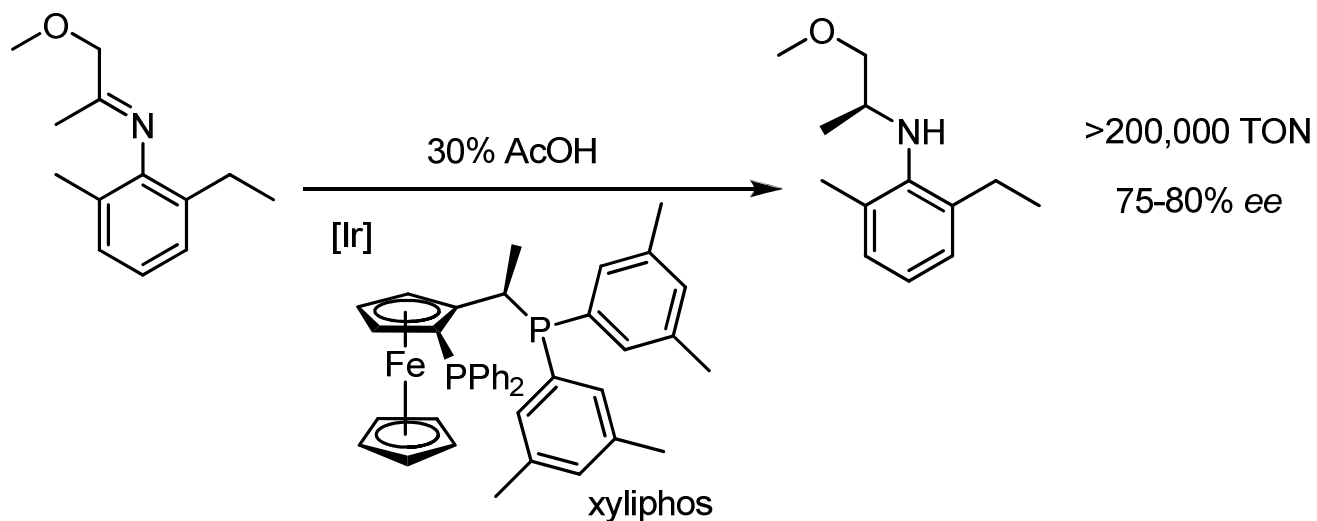
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Blaser, H-U. *Adv. Synth. Catal.* **2002**, *334*, 17-31.

Blaser, H-U.; Pugin, B.; Splinder, F.; Thommen, M.; *Acc. Chem. Res.* **2007**, *40*, 1240-1250.

# The Final Breakthrough – The Magic of AcOH

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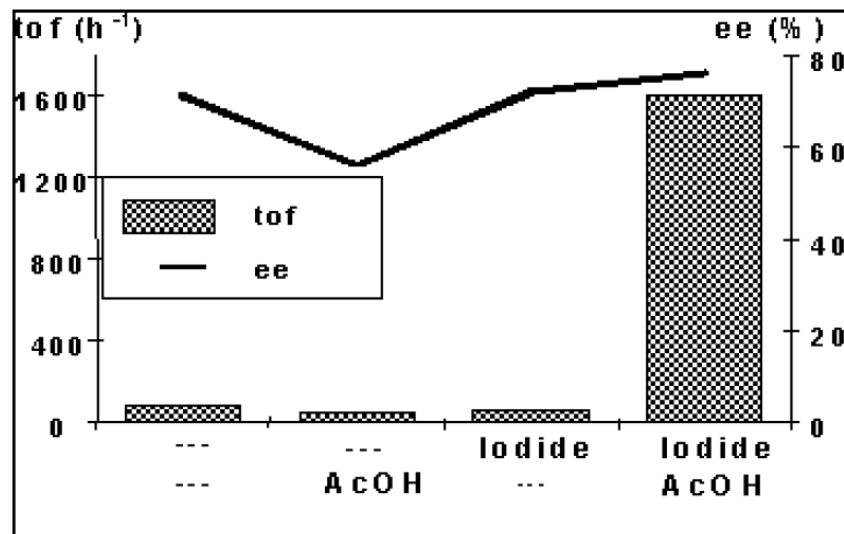


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Blaser, H-U. *Adv. Synth. Catal.* **2002**, 334, 17-31.

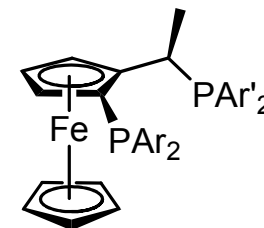
Blaser, H-U.; Pugin, B.; Splinder, F.; Thommen, M.; *Acc. Chem. Res.* **2007**, 40, 1240-1250.

# Exceeding all expectations – by quite a margin!



Over 30 different diphosphine ferrocenyl ligands screened.

Ar	Ar'	TON	TOF (h <sup>-1</sup> )	ee
Ph	3,5-xylyl	1,000,000	>200,000	79
<i>p</i> -CF <sub>3</sub> C <sub>6</sub> H <sub>6</sub>	3,5-xylyl	800	400	82
Ph	4- <sup>t</sup> Bu-C <sub>6</sub> H <sub>4</sub>	5,000	80	87
Ph	4-( <sup>n</sup> Pr) <sub>2</sub> N-3,5-xylyl	100,000	28,000	83



Blaser, H-U. *Adv. Synth. Catal.* **2002**, 334, 17-31.

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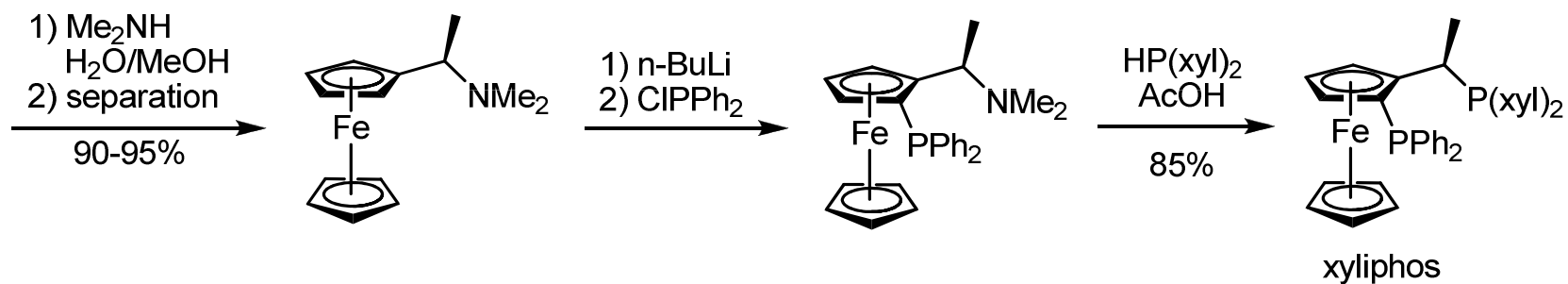
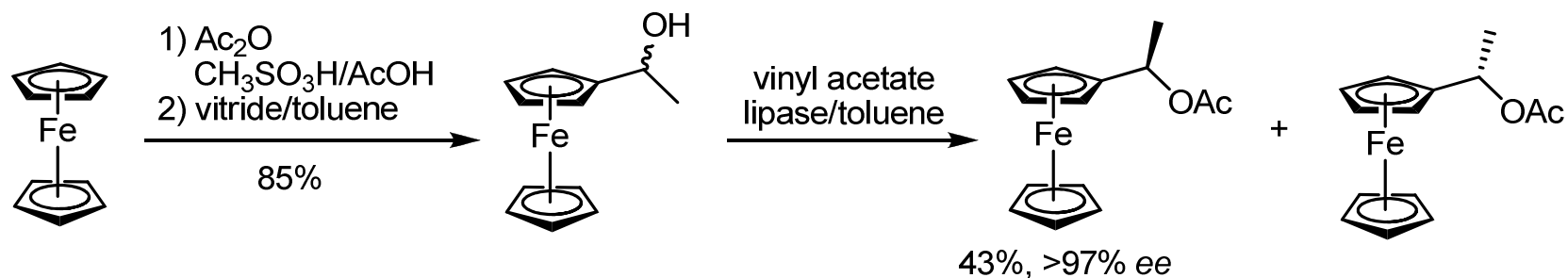
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Blaser, H-U. *Adv. Synth. Catal.* **2002**, *334*, 17-31.

Blaser, H-U.; Pugin, B.; Splinder, F.; Thommen, M.; *Acc. Chem. Res.* **2007**, *40*, 1240-1250.



# From Lab to Plant – Technical Ligand Synthesis



Synthesis in 2500 L reactors

Hundreds of kg scale

>99.5% ee

# The Loop Reactor & the Plant, Kaisten, Switzerland (Syngenta)

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## Post hydrogenation

Continuous aqueous extraction to neutralize and eliminate acid from crude.

Flash distillation to remove residual water.

Subsequent distillation to remove water from catalyst on a thin film evaporator.

Residue – Ir is recovered, ligand is lost.

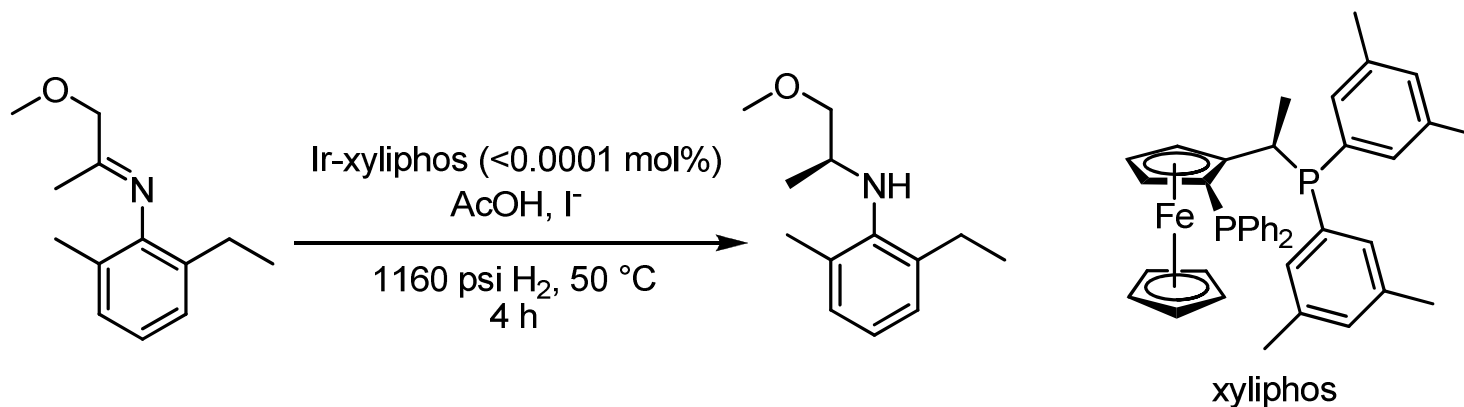
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Hofer, R. *Chimia* **2005**, *59*, 10-12.

Blaser, H-U. *Adv. Synth. Catal.* **2002**, *334*, 17-31.

# The Final Production Process

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100% conversion  
79% ee  
>7,000,000 TON  
>2,000,000 TOF (h<sup>-1</sup>)

34 g Ir complex + 70 g xylyphos ligand + some acid + some iodide  
gives

10,000 kg of hydrogenated product, 79% ee, 4 h

>10,000 tons/year scale commercial production till date in Switzerland  
(Syngenta)

# The Key Development Team (top-bottom, left-right)



## Benoit Pugin

1981 – PhD, Prof. Venanzi (ETH, Zurich),  
1982/3 – Post-doc at Ciba-Geigy  
1983... – Ciba-Geigy, Novartis and presently at Solvias  
Development of new chiral ligands for asymmetric catalysis

## Hans-Ulrich Blaser (the chief)

1971 – PhD, Prof. Eschenmoser (ETH, Zurich)  
1971/5 – Post-docs at U. Chicago (J. Halpern), Harvard U.  
(J. Osborn), Monsanto (Zurich)  
1976-96 – Ciba-Geigy.  
1996-99 – Novartis  
1999... – Solvias  
Industrial application of selective catalysts

## Felix Splinder

1981 – PhD, Prof. Venanzi (ETH, Zurich)  
1983-96 – Ciba-Geigy  
1996-99 – Novartis  
1999... - Solvias  
Homogenous enantioselective hydrogenation

## Hans-Peter Jalett

Solvias – Chief technician in Catalysis Section

# AcOH was the magical key

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AcOH as an additive was common in heterogenous catalysis, never investigated in homogenous catalysis.

In fact, Benoit Pugin had found negative effects of AcOH with the Ir-diop ligands in 1986.

Most specialists would have dissuaded Hans-Peter Jalett...

*...but he never asked!*

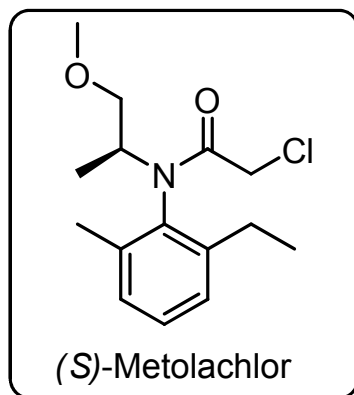
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*“...faced with a decision based solely upon hypothetical arguments, consider all reasons not to perform an experiment, and disregard them.”*

– R. B. Woodward  
as heard from J. Woods  
(2009, Michigan State U.)

# The Glory of the (S)-Metolachlor Odyssey

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- (S)-metolachlor is the active ingredient in Dual Magnum<sup>®</sup>, one of the most important grass herbicides for use in maize.
- Key step in synthesis – an Ir-catalyzed asymmetric hydrogenation.
- A 14 year odyssey of development.
- Operated on a >10,000 ton/year scale since 1996.
- This is to date the largest application of asymmetric catalysis.
- The Ir-Xyliphos is the most active and productive catalyst till date (>7,000,000 TON and >2,000,000 TOF).
- Developed during the incipient years of asymmetric hydrogenation – a historical case study.



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